EFFECTS OF THE INITIAL SIZE OF WATER DROPLET ON ITS EVAPORATION ON HEATED SURFACES

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(Received 14 October 1978)

NOMENCLATURE

- projected base area of droplet $[m^2]$; $\frac{A}{\overline{A}},$ time-averaged projected base area of droplet
- $[m^2]$;
- D_0 initial diameter of droplet [m] ;
- temperature T_{w0} having the maximum T_r , evaporation time, i.e. Leidenfrost temperature $[°C];$
- $T_{\rm sat}$ saturation temperature $[°C]$;
- T_{w0} ,
 T_{ws} ,
 ΔT_{su} , initial surface temperature $\lceil {^{\circ}C} \rceil$;
- time-averaged surface temperature $[°C]$;
- $= T_{ws} T_{sat}$ [K]; Q, heat required to evaporate completely one droplet $[J]$;

q, time-averaged heat flux,
$$
q = \frac{Q}{\bar{A}\tau} [W/m^2];
$$

total evaporation time [s]. τ.

IN THE previous paper [I], we discussed the heat-transfer characteristic of evaporation of a single droplet of pure water on various heated plates (materials: copper, brass, carbon steel and stainless steel), by correlating the timeaveraged heat flux q with the time-averaged surface superheating of plate ΔT_{sat} , which were obtained from timedependent measurements of the surface temperature of plate just below the droplet and the projected base area A of the droplet. In that case, we dealt with the droplet whose initial diameter D_0 was 3.29 mm in the range of initial surface temperature T_{w0} less than the Leidenfrost temperature T_F , while we used four initial droplet sizes, 2.54, 2.78, 2.86 and 3.29 mm dia in the range of $T_{w0} > T_F$.

In this note, three initial droplet sizes, 2.54, 2.86 and 4SOmm dia, are dealt with in addition to 3.29mm in the range of $T_{w0} < T_F$. The initial temperature of water droplet is about 20°C. The experimental apparatus and procedure, and also the correlation technique are the same as those described in the previous paper $[1]$. Recent works $[2-10]$ are concerned with the evaporation of liquid droplet on the heating surface and with the liquid-liquid thermal interaction.

Examples of the total evaporation time τ correlated with the initial surface temperature T_{w0} are shown in Fig. 1(a) and (b). Measurements of τ are conducted by increasing stepwise the initial surface temperature T_{w0} from room temperature to higher temperature, which is called UP, and thereafter they are conducted by decreasing stepwise from the high temperature to lower temperature, which is called DOWN. If we represent the same data as those in Fig. 1 on the q vs T_{ws} diagram after the correlation technique treated in the previous paper, we can get Fig. 2(a) and (b). It can be seen that two figures coincide very well when the temperature T_{ws} is less than about 120 \degree C, regardless of UP and DOWN, material of heated plate and initial droplet diameter D_0 .

FIG. 1. Total evaporation time τ vs initial surface temperature T_{w0} : (a) copper, $D_0 = 2.54$ mm; (b) stainless steel, D_0 $= 4.50$ mm.

Figure 3(a) and (b) illustrate the so-called boiling curve (q vs ΔT_{sat} diagram) and they show the nucleate boiling and transition boiling regions. Although there is a little scatter of experimental data, the effect of D_0 on the boiling curve can not be recognized.

FIG. 2. Time-averaged heat flux q vs time-averaged surface temperature T_{ws} : (a) copper, $D_0 = 2.54$ mm; (b) stainles steel, *D, = 4.50* mm.

Corresponding to Fig. I3 in the previous paper, all of our data are represented in Fig. 4 without distinction of *D,.* From this figure, the following conclusion can be derived. In the nucleate boiling region, our present data obtained by using the droplet of $D_0 = 2.54 - 4.50$ mm seem to provide a straight line parallel to the nucleate pool boiling curve for thin water film (see $[11-13]$), no matter what material is used for heated plate and no matter which size of droplet is used for the initial diameter. Our present data are more close to Shibayama et al.'s recent experimental data [11], which were obtained by using thin water film of 2 mm thickness on the horizontal heating surface of 22mm dia. than other investigators' data $[12, 13]$. This might be due to the fact that Shibayama et al. conducted the experiment of nucleate boiling on the heating surface of small area as compared with other investigators'.

In the transition boiling region, the curve for the heated plate of lower thermal diffusivity (stainless steel) comes to higher $\Delta T_{\rm sat}$ than for higher thermal diffusivity (copper) independently of *D,.* This corresponds to the fact that the higher the thermal diffusivity of the plate, the lower the Leidenfrost temperature T_F (see Fig. 2 in [1]).

In the film boiling region, the effect of initial droplet diameter on the heat-transfer characteristic has been already discussed in the previous paper, and the relation between q and ΔT_{sat} is almost independent of D_0 .

FIG. 3. Effects of initial droplet diameter D_0 on the boiling curve: (a) copper; (b) carbon steel.

FIG. 4. Boiling curve for various heated plates, $D_0 = 2.54 - 4.50$ mm.

REFERENCES

- 1. I. Michiyoshi and K. Makino, Heat transfer character istics of evaporation of a liquid droplet on heated surfaces, Int. J. *Heat* Mass *Transfer* 21,605-613 (1978).
- \mathfrak{Z} S. Toda, *Heat Transfer in Mist* Cooling, *Developments in 9.* Heat Transfer, (Dennetsu Kogaku no Shinten), Vol. 3, pp. *2* I *I-330.* Yokendo, Tokyo (1974).
- 3. M. Seki, H. Kawamura and K. Sanokawa, Transient temperature profile of a hot wall due to an impinging liquid droplet, *J. Heat Transf.* **100C**, 167-169 (1978).
- 4. M. Seki. H. Kawamura and K. Sanokawa, Unsteady state heat transfer of impinging droplets-1st Report. Measurements of change in temperature of heated surface, in *Proceedings of the Ninth Japan Heat Trarlsfer Symposium,* pp. 459-462. Heat Transfer Society of Japan, Tokyo (1972).
- 5. S. Nishio and M. Hirata, Study on the Leidenfrost temperature- 1st Report. Experimental study on the fundamental characteristics of the Leidenfrost temperature, *Trans. Japan Soc. Mech. Engrs* 43(374), *385\$-3867 (1977):*
- 6. S. Nishio and M. Hirata, Study on the Leidenfrost 13. temperature-2nd Report. Behavior of liquid-solid contact surface and Leidenfrost temperature, *Trans.* Japan Soc. Mech. Engrs 44(380), 1335-1346 (1978).
- 7. M. Mizomoto, H. Hayano and S. Ikai, Evaporation and ignition of a fuel droplet on a hot surface-1st Report. Evaporation, *Trans. Japan Sot.* Mech. *Engrs* 44(380), 1366-1373 (1978).
- M. Mizomoto, H. Hayano and S. Ikai, Evaporation and ignition of a fuel droplet on a hot surface-2nd Report. Ignition, *Trans. Japan Sot.* Mech. *Engrs* 44(380), 1374-1382 (1978).
- V. H. Arakeri, I. Catton, W. E. Kastenberg and M. S. Plesset, Thermal interaction for molten tin dropped into water, Int. *J. Heat Mass Transfer* 21, 325-333 *(1978).*
- A. G. Newlands and W. D. Halstead, The reaction between water droplets and molten sodium, *Int. J. Heat Mass Transfer 21. 897-903 (1978).*
- S. Shibayama, M. Katsuta, K. Suzuki, T. Kurose and Y. Hatano, A study on boiling heat transfer in thin liquid film-1st Report. In the case of pure water and aqueous solution of surface active-agents as working fluid, *Trans. Japan Sot.* Mech. *Engrs* 44(384), 2429-2438 (1978).
- 12. I. Michiyoshi and N. Ueno, Heat transfer to thin water film, in *Proceedings of the Ninth Japan Heat Transfer* Symposium, pp. 185-188. Heat Transfer Society of Japan, Tokyo (1972).
- 13. H. Kusuda and K. Nishikawa, Boiling heat transfer in the liquid film-1st Report. The effect of physical properties of the liquid and the condition of the heating surface, *Trans. Japan Soc. Mech. Engrs* 34(261), *935-943 (1968).*
- W. H. Jens and P. A. Lottes, Analysis of heat transfer burnout, pressure drop and density data for high pressure water, ANL-4627 (1951).